

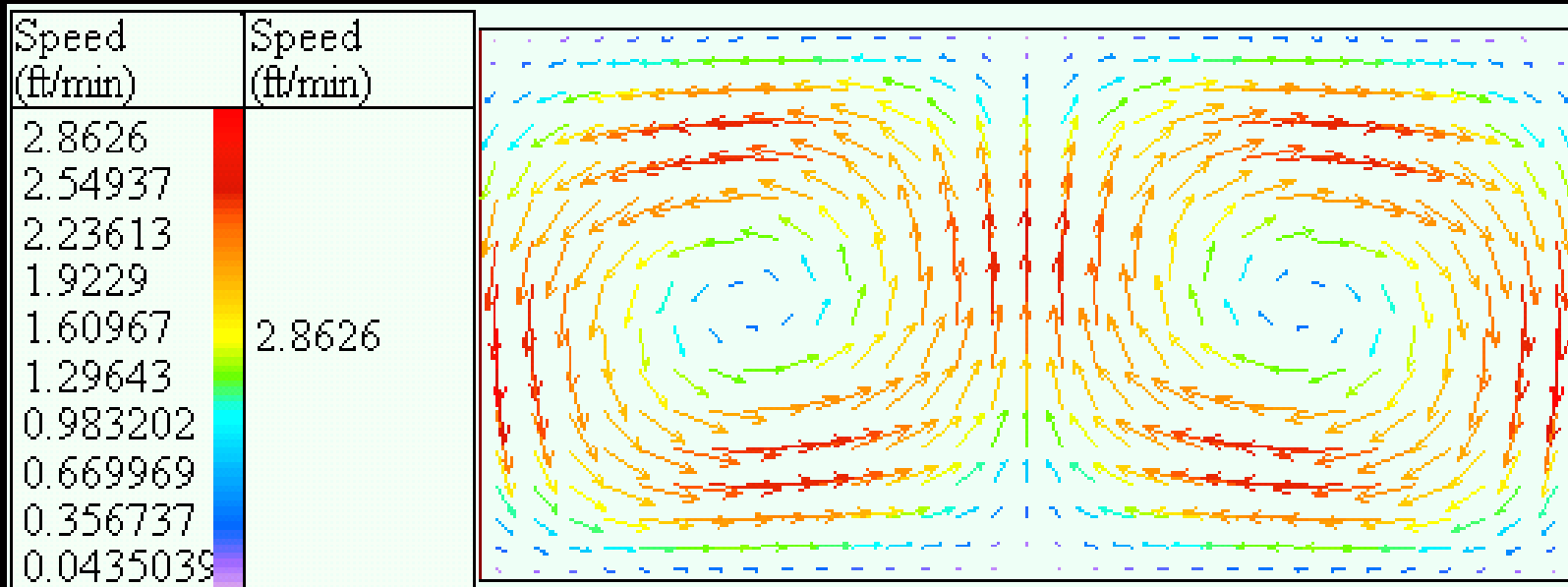
Validation Cases

www.resheji.com

© Flomerics Ltd 2001

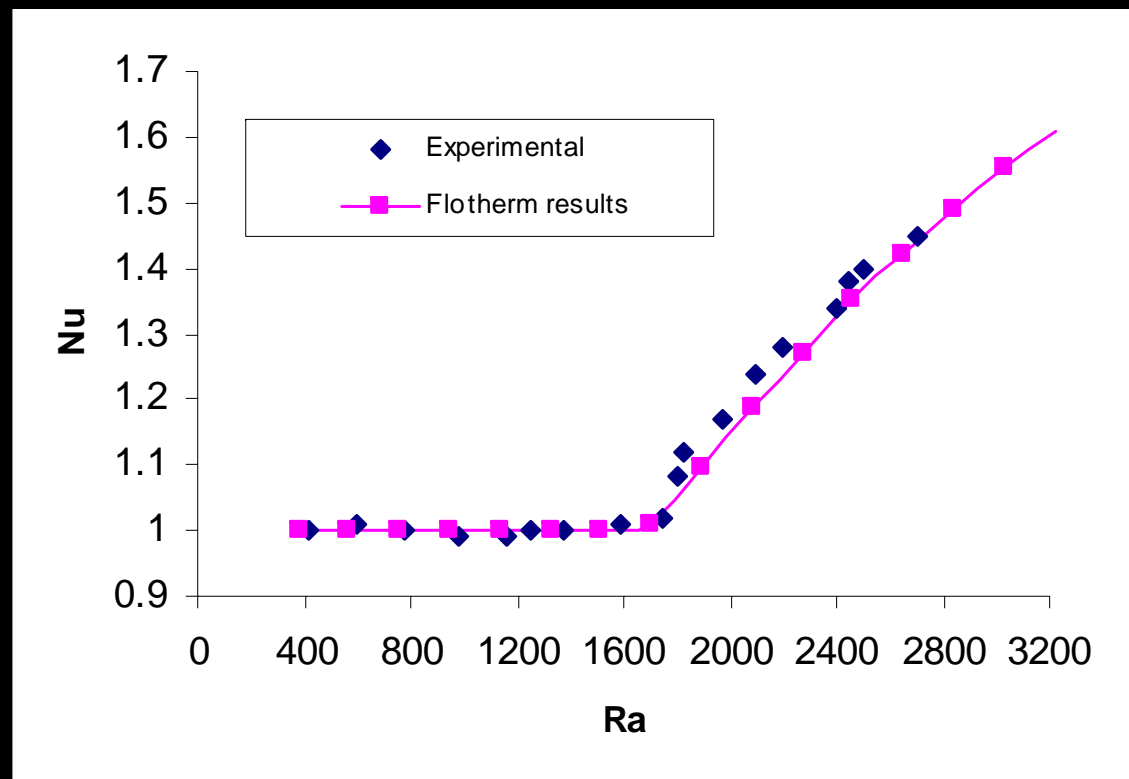
Bernard Convection

- ▶ Cold wall above, Hot Wall below



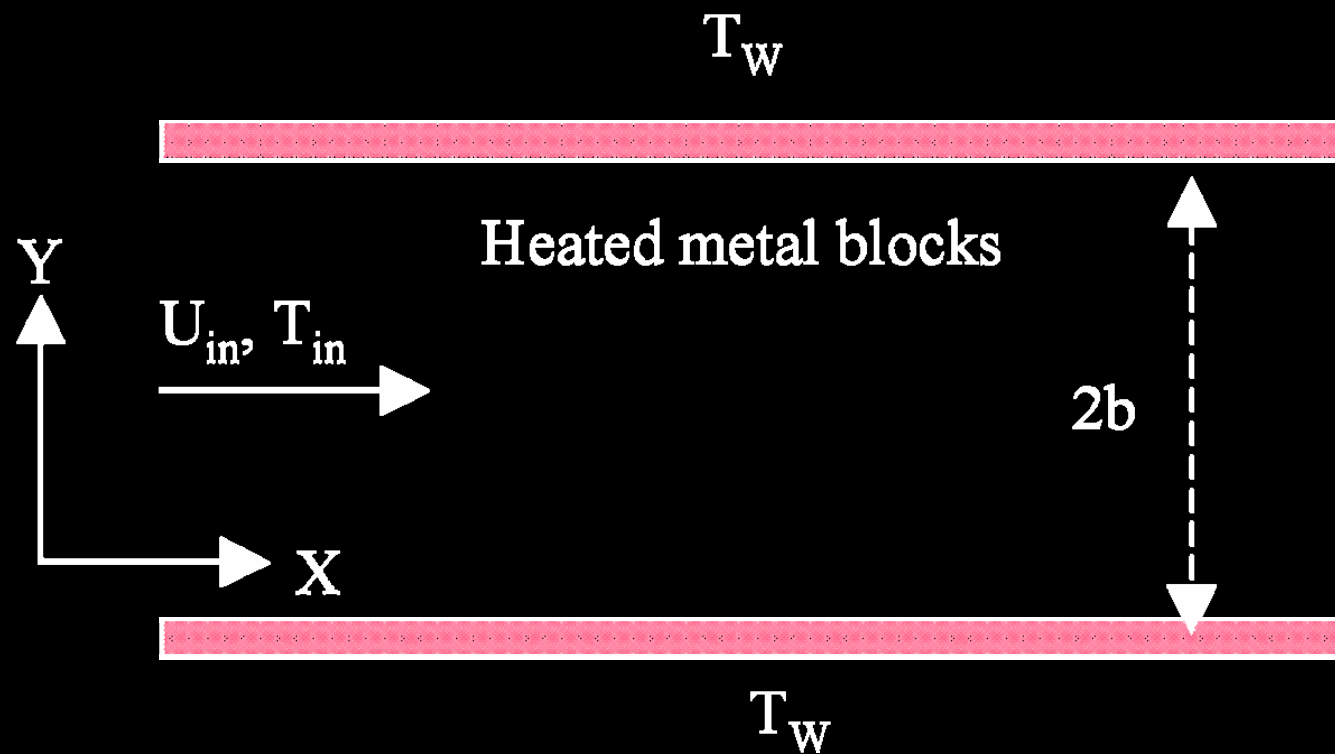
Bernard Convection

► Results:



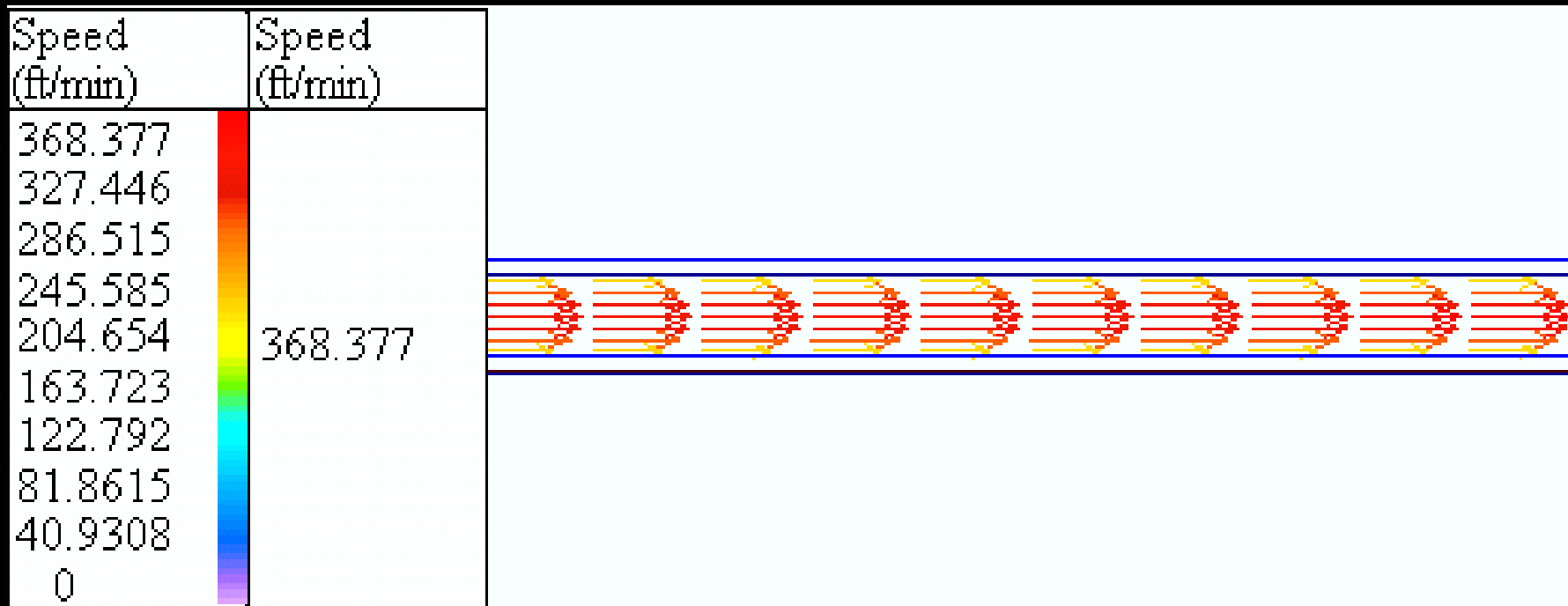
Flat Plates

► Geometry:



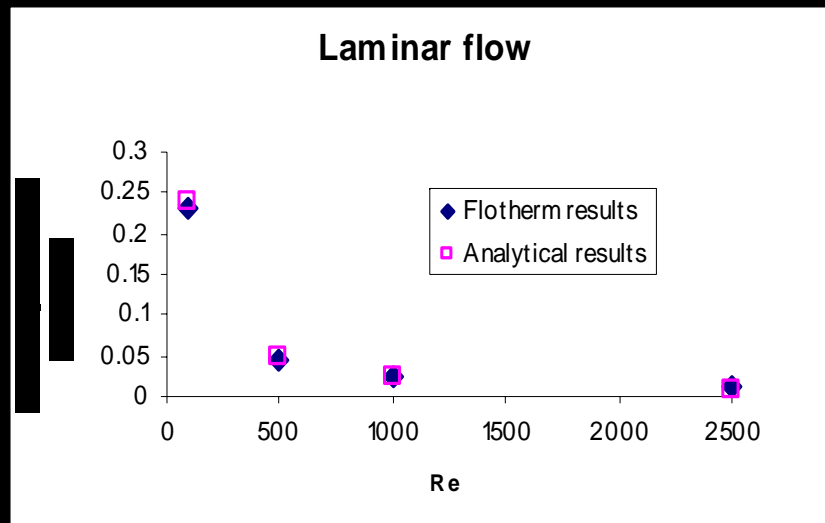
Flat Plates

▶ FLOTHERM:

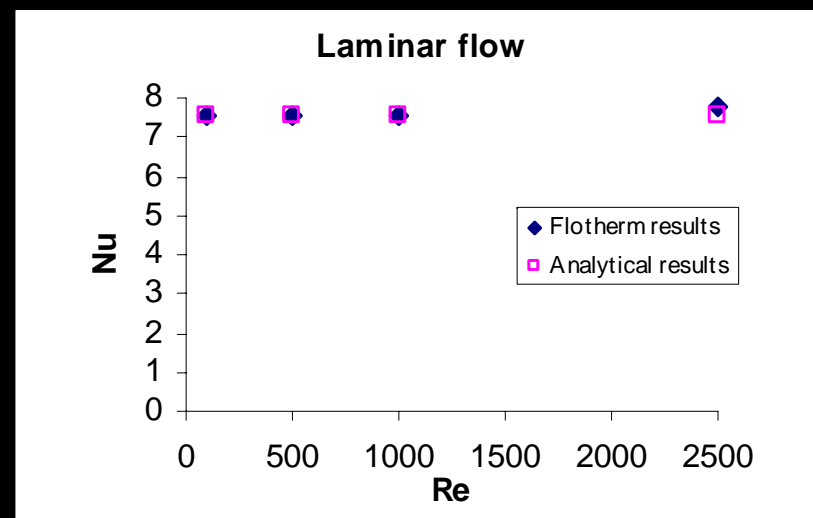


Flat Plates - Laminar

- ▶ Comparison with analytical results:



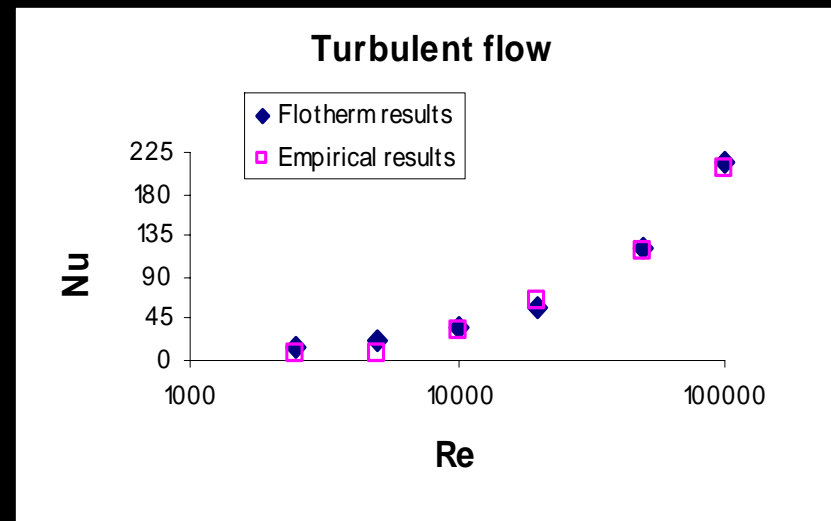
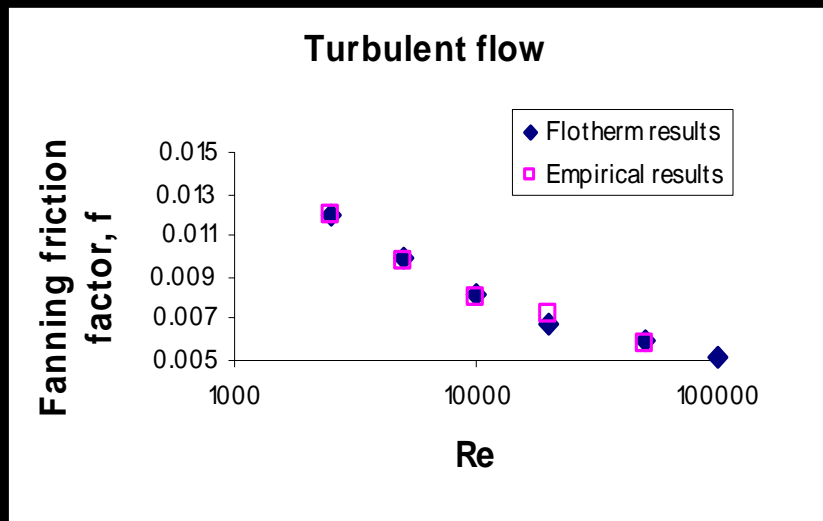
$$f = \frac{24}{Re}$$



$$Nu = 7.54$$

Flat Plates - Turbulent

- ▶ Comparison with empirical results:



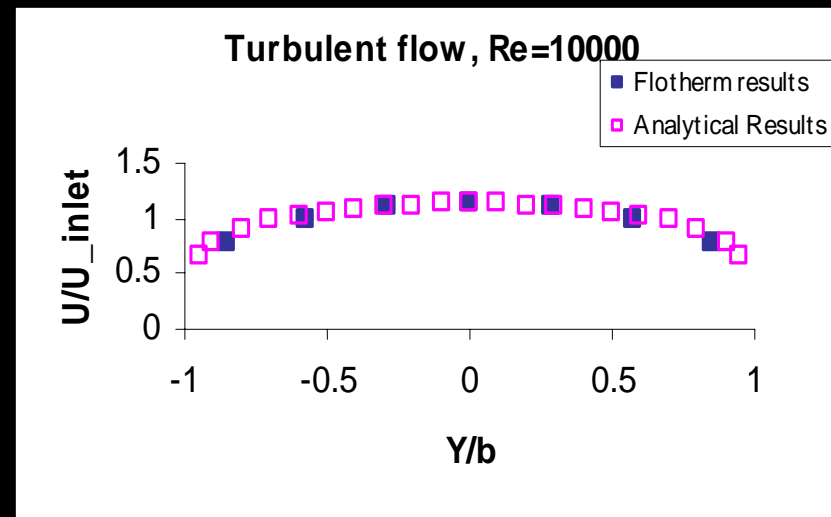
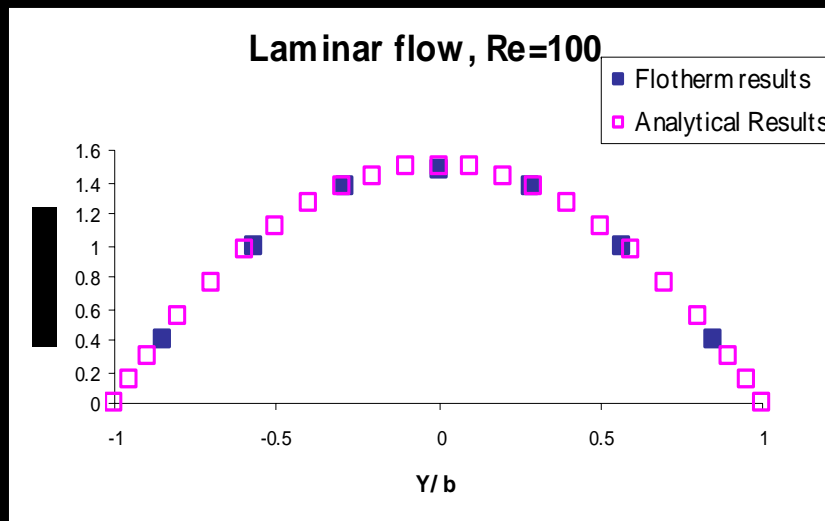
$$f = \frac{0.1268}{Re^{0.3}} \quad 5000 < Re < 30000$$

$$f = \frac{0.0868}{Re^{0.25}} \quad 12000 < Re < 1.2 \times 10^6$$

$$Nu = 0.023 Re^{0.8} Pr^{0.3}$$

Flat Plates

► Flow profiles



► Analytical

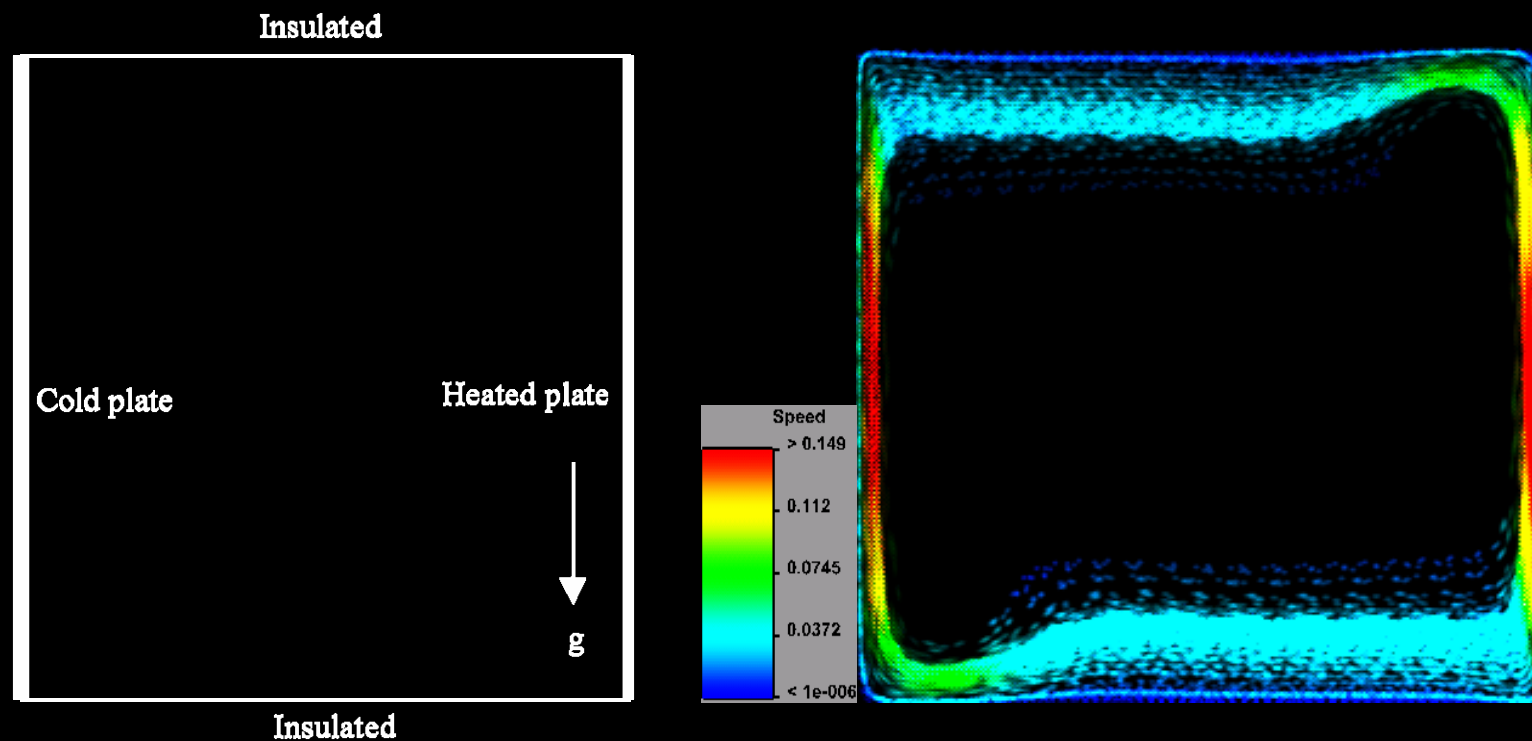
$$\frac{U}{U_{in}} = \frac{3}{2} \left(1 - \left(\frac{y}{b} \right)^2 \right)$$

► Empirical

$$\frac{U}{U_{in}} = 1 + \left(\frac{f}{2} \right)^{0.5} / K_2 \left(\frac{5}{6} + \log \left(1 - \left(\frac{y}{b} \right)^{0.5} \right) + \left(\frac{y}{b} \right)^{0.5} \right)$$

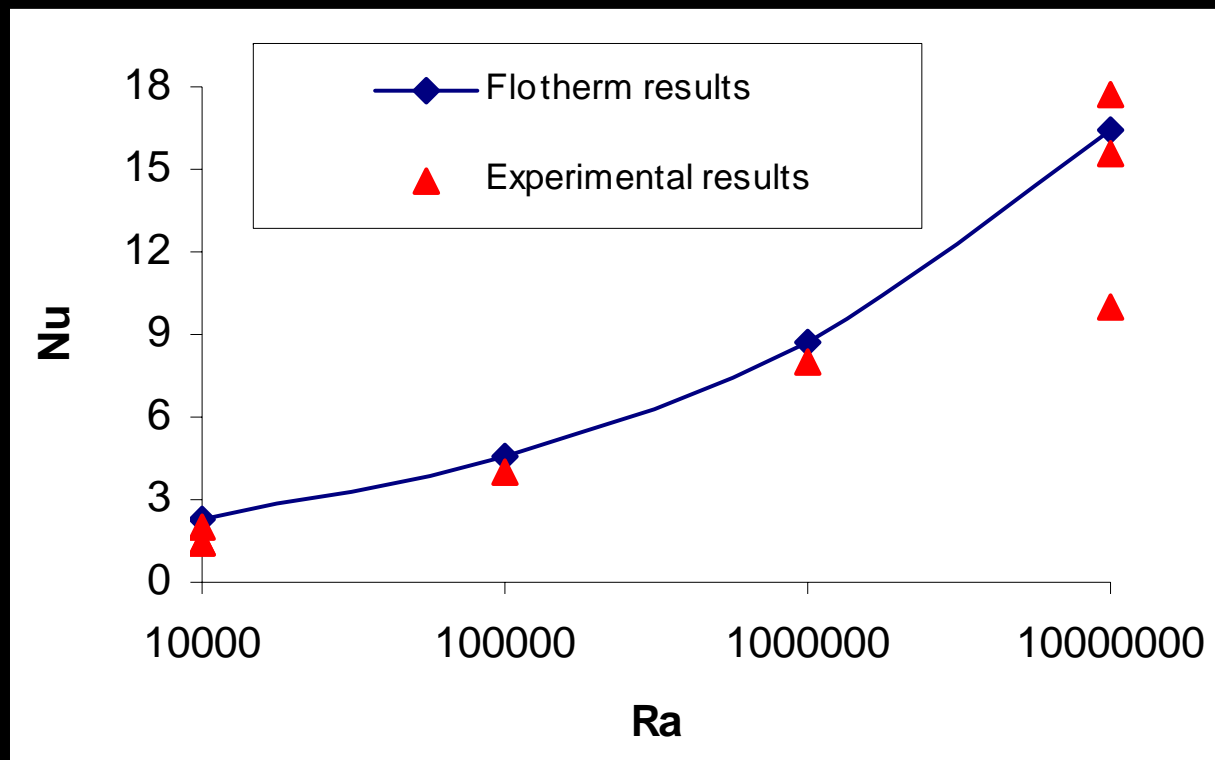
Closed Cavity

- ▶ Heat transfer by natural convection



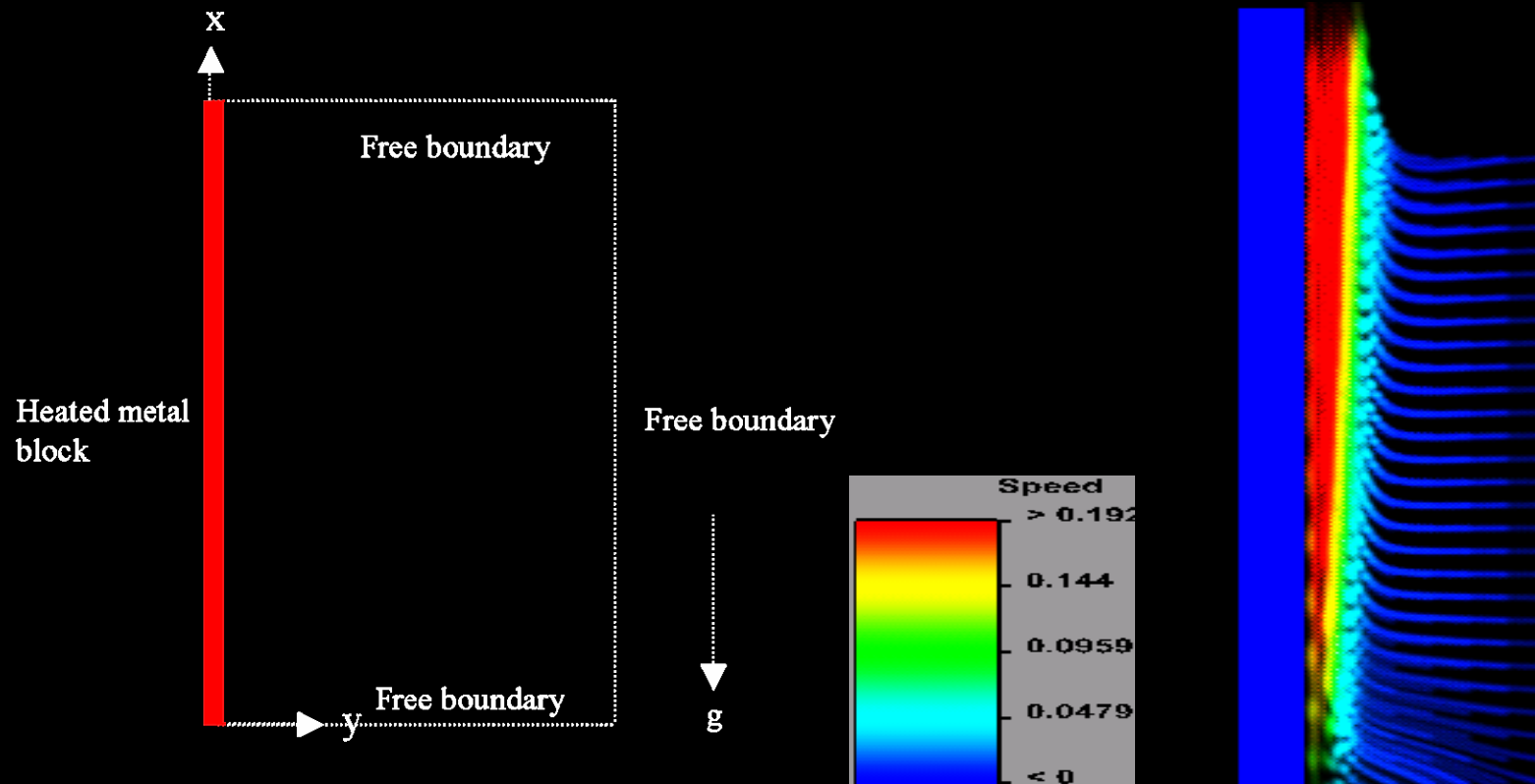
Closed Cavity

► Nusselt vs Rayleigh Number



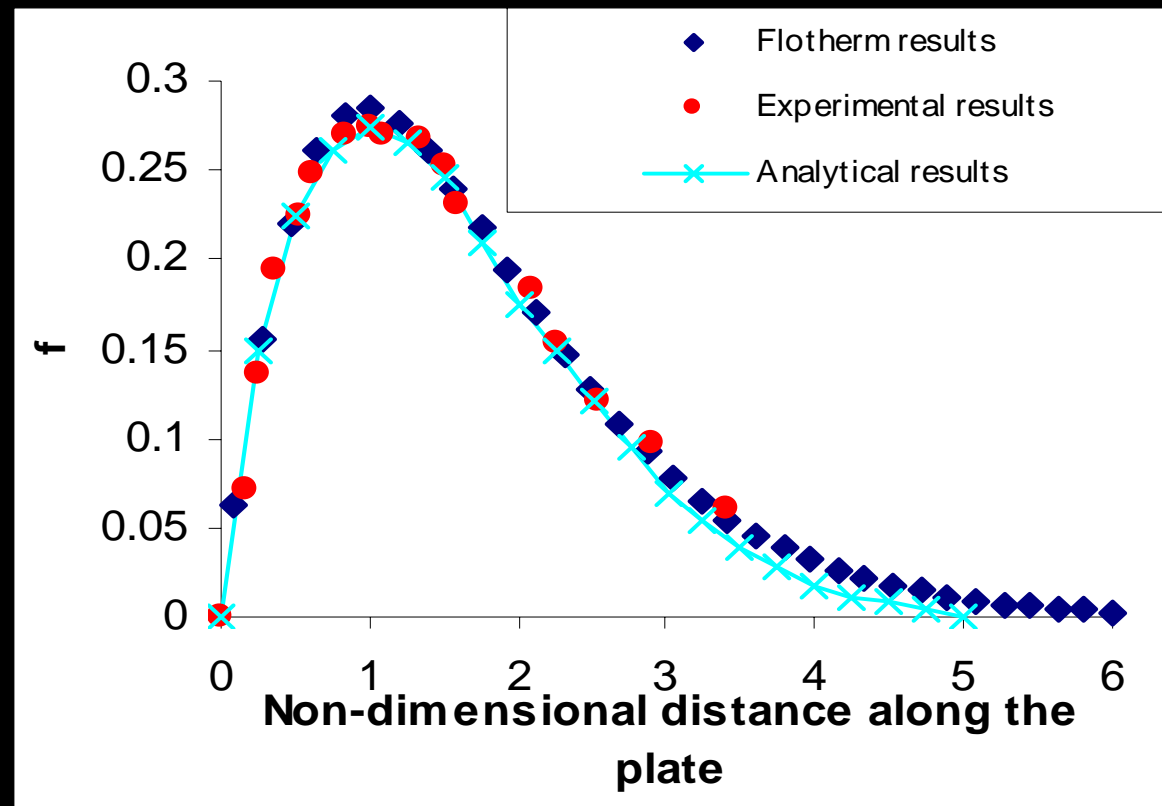
Vertical Plate

► Natural Convection



Vertical Plate

▶ Dimensionless velocity, f



Vertical Plate

► Dimensionless temperature

