

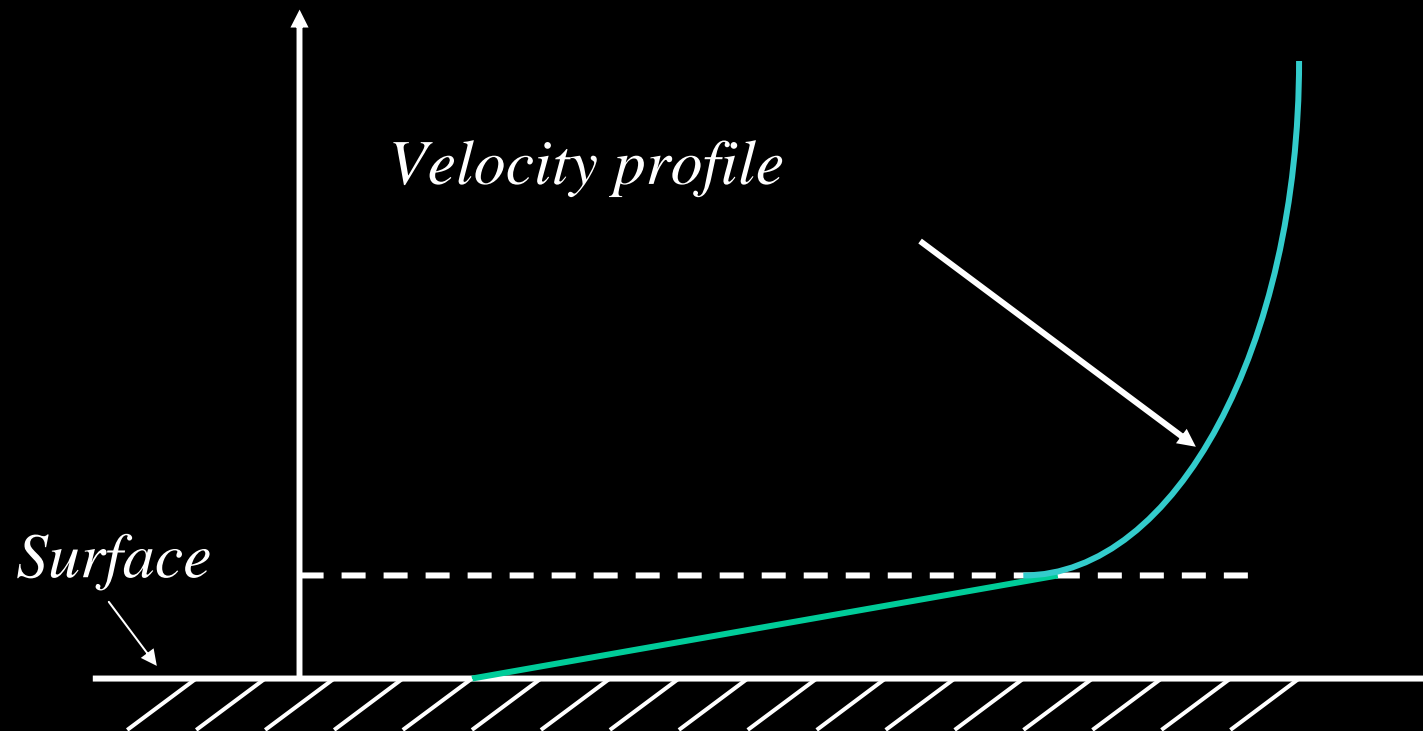
# Boundary Layers and Heat Transfer

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# Velocity Boundary Layer

Along the solid surface, the fluid velocity varies from  $V_\infty$  to zero at the wall  $\Rightarrow$  velocity boundary layer  $\delta$



# Near Wall Treatments

- The boundary layer is a very complex region of high velocity gradient and diffusion dominated development.
- To model it precisely would necessitate an extremely fine grid.
- An empirical relationship is therefore used to describe the shape of the boundary layer so that only one grid cell near the wall is required

# Near Wall Treatments

- Friction velocity

$$u_{\tau} = \sqrt{\frac{\tau_w}{\rho}}$$

- Distance

$$y^+ = \frac{\rho u_{\tau} y}{\mu}$$

- Velocity

$$u^+ = \frac{u}{u_{\tau}}$$

# Near Wall Treatments

- Relationship for smooth walls

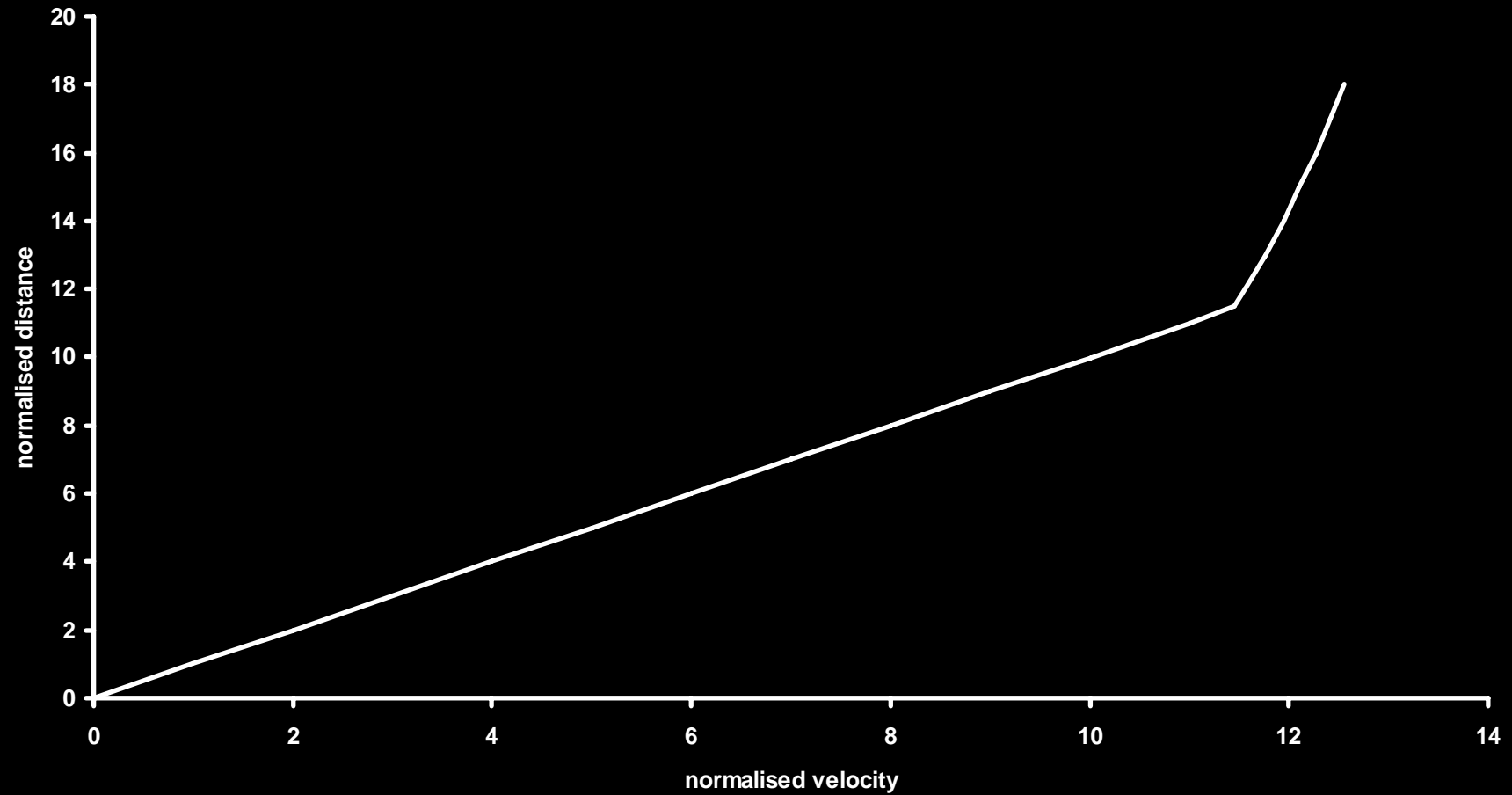
*Laminar sub-layer :*

$$u^+ = y^+$$

*Turbulent boundary layer :*

$$u^+ = \frac{1}{0.435} \ln(9y^+)$$

# Graph of $u^+$ vs $y^+$



# Modelling

- Fine grid to resolve thermal and velocity gradients
- Not too fine
- For KE turbulence model, first cell centre MUST be outside laminar sub-layer

# First Cell

- Can find  $y^+$  from results in first cell.
- Take velocity parallel to wall

$u$

- Get half-cell height

$y$

- Now, product of these:

$y u$



# First Cell

- Product  $u^+y^+$  can be found

$$u^+y^+ = \frac{\rho u y}{\mu}$$

- Must now iterate to find  $y^+$
- If  $u^+y^+ > 132$ , then flow is turbulent

# Heat Transfer

- For smooth walls, heat transfer rate per unit area is related to the 'Stanton number':

$$St = \frac{\dot{Q}_w}{\rho U C_p (T - T_w)}$$

# Heat Transfer

- Laminar flow

$$St = \frac{1}{Re Pr}$$

$$\dot{Q}_w = \frac{k}{y} (T - T_w)$$

- Conduction into the fluid

# Heat Transfer

- Turbulent flow
- Use Taylor-Prandtl analogy (heat flux is proportional to momentum flux)

$$St = \frac{s}{0.9 \left( 1 + s^{1/2} P_j \right)}$$

# Heat Transfer

- Turbulent Prandtl number = 0.9

$$s = \frac{\tau_w}{\rho u^2}$$

$$P_j = 9 \left( \frac{Pr}{0.9} - 1 \right) \left( \frac{0.9}{Pr} \right)^{1/4}$$

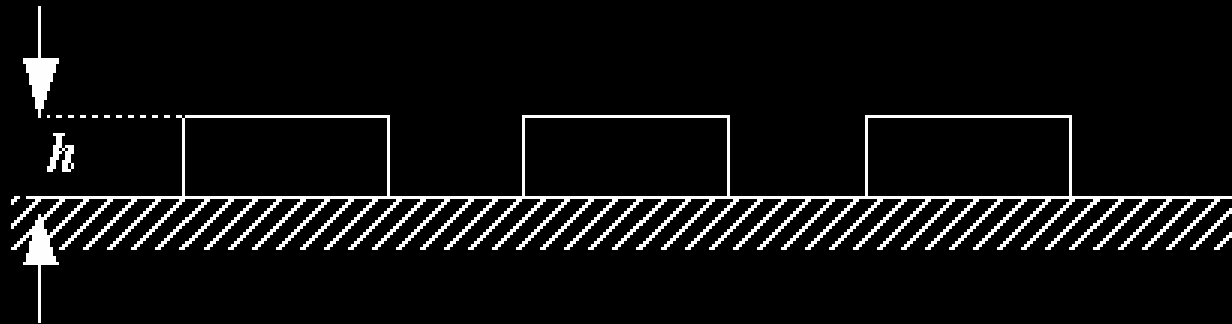
- Jayatilleke's sub-layer resistance function

# Heat Transfer

- Stanton number is determined depending on  $y^+$  in the near wall cell
- Heat transfer rate is then determined based on temperature difference
- This heat is transferred from solid cell to fluid cell

# Near Wall Treatments

- Rough walls



$$Re_r = \frac{\rho h u_\tau}{\mu}$$

# Friction

- $Re_r$  = 'roughness Reynolds number'
- If  $Re_r < 3.3$  treat as smooth, otherwise:

$$\frac{u}{u_\tau} = \frac{1}{0.435} \ln\left(\frac{29.7y}{h}\right)$$

- Calculate  $u_\tau$  and hence  $\tau_w$  (wall shear stress)